

(19) World Intellectual Property Organization  
International Bureau



(43) International Publication Date  
8 May 2003 (08.05.2003)

PCT

(10) International Publication Number  
**WO 03/037989 A1**

- (51) International Patent Classification<sup>7</sup>: C08L 101/00, 71/00, C09D 7/00
- (21) International Application Number: PCT/US02/32323
- (22) International Filing Date: 9 October 2002 (09.10.2002)
- (25) Filing Language: English
- (26) Publication Language: English
- (30) Priority Data:  
10/003,755 29 October 2001 (29.10.2001) US
- (71) Applicant: **HERCULES INCORPORATED** [US/US];  
Hercules Plaza, 1313 North Market Street, Wilmington, DE  
19894-0001 (US).
- (81) Designated States (*national*): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, OM, PH, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TN, TR, TT, TZ, UA, UG, UZ, VN, YU, ZA, ZM, ZW.
- (84) Designated States (*regional*): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, SK, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).
- (72) Inventor: SAU, Arjun, C.; 521 Langwater Drive, Newark, DE 19711 (US).
- Published:  
— with international search report
- (74) Agent: **EDWARDS, David**; Hercules Incorporated, Hercules Plaza, 1313 North Market Street, Wilmington, DE 19894-0001 (US).
- For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.*

(54) Title: SUPPRESSION OF AQUEOUS VISCOSITY OF ASSOCIATING POLYACETAL-POLYETHERS

(57) Abstract: A composition is composed of a hydrophobically modified polyacetal- polyether (HM-PAPE) or comb hydrophobically modified polyacetal-polyether (comb HM-PAPE) and a viscosity suppressing agent of cyclodextrins or derivatives thereof. A method for improving the pumpability and pourability of aqueous solutions of HM-PAPE or comb HM-PAPE is provided by admixing a cyclodextrin with the HM-PAPE or comb HM-PAPE to form a complex of the cyclodextrin and HM-PAPE or comb HM-PAPE where the viscosity of the HM- PAPE or comb HM-PAPE is suppressed and adding the complexed admixture to an aqueous system containing a water-insoluble polymer wherein the cyclodextrin is decomplexed and the HM-PAPE or comb HM-PAPE becomes an effective thickener. An example of the uses for this composition and method is in film forming coatings such as latex paints.



WO 03/037989 A1

## **SUPPRESSION OF AQUEOUS VISCOSITY OF ASSOCIATING POLYACETAL-POLYETHERS**

### **Field of the Invention**

This invention relates to controlling the solution viscosity and other rheological properties of associative thickeners in aqueous media. More particularly, this invention relates to aqueous formulations of hydrophobically modified polyacetal-polyethers (HM-PAPEs) and cyclodextrins to suppress and control the solution viscosity of such thickeners. This invention also relates to the use of these associative thickener formulations in systems that are to be thickened such as water-borne paints.

### **BACKGROUND OF THE INVENTION**

Highly filled aqueous systems, such as water-borne coatings (latex or emulsion paints), inks, construction materials, and cosmetics are formulated with hydrophobically modified water-soluble polymers (HM-WSPs) to control the rheology of coatings during manufacturing, storage and applications. These HM-WSPs are commonly referred to in the art as "associative thickeners". They are so called because they thicken the latex paints by forming a three-dimensional network through intermolecular associations of the hydrophobic moieties present in the HM-WSP chains and/or with other hydrophobic components present in the coatings formulation. Water-borne architectural coatings are used for on-site application to interior or exterior surfaces of residential, commercial, institutional, or industrial buildings. Associative thickeners have become the industry standards as the rheology modifiers in paints because they have a number of advantages over conventional thickener systems. These include: (1) a lower viscosity during incorporation, (2) a lower tendency to spatter during application, (3) good flow and leveling upon application, (4) better color, (5) higher gloss through less flocculation, (6) lower sensitivity of the coatings to water, (7) less vulnerability to microbial degradation, and (8) minimal reduction in the viscosity of the thickened dispersions on exposure to shearing (approaching Newtonian flow behavior).

These associative thickeners are normally sold as high solids solutions in water or a mixture of water and an organic cosolvent, such as butyl carbitol or propylene glycol. The function of these cosolvents is to suppress the viscosity of the aqueous solution containing the associative thickener to allow for ease of handling before it is used as a thickener. While these organic cosolvents perform their intended function, they possess potential environmental, safety, and health problems. These organic cosolvents contribute to volatile organic compounds (VOCs) which are not environmentally friendly. Since these VOCs potentially harm the atmosphere, environmentalists are getting bills passed in the Government in order to reduce the VOCs emitted into the atmosphere. Hence, companies that produce or market formulations that produce large volumes of VOCs are being required either to reduce the level of VOCs or to eliminate them all together. Companies in the paint industry are now concerned about VOCs and are asking their suppliers to provide environmentally friendly products with low or no VOCs.

One approach to suppress the aqueous viscosity of associative thickeners and yet be environmentally friendly is to use surfactants in the paint. Although this presents no specific health or environmental hazard, it does degrade formulation performance. US Patent No. 6,150,445 describes the use of nonionic surfactants in small amounts, which owing to their micelle-forming capability can reduce the viscosity of the aqueous concentrate of the associative thickener.

25

Another approach is described in US Patent Nos. 5,137,571 and 5,376,709 that disclose the use of cyclodextrins or their derivatives to suppress the solution viscosity of hydrophobically modified ethoxylated polyurethanes, hydrophobically modified alkali-soluble emulsions, hydrophobically modified hydroxyethylcellulose, or hydrophobically modified polyacrylamides.

30

Another approach is to reduce the molecular weight of the associative thickener so that no viscosity suppressant is needed to prepare high solids solutions in water with manageable viscosity.

5           Recently, the compositions and applications of a new class of associative thickeners based on hydrophobically modified polyacetal (ketal)-polyether were described in US Patent Nos. 5,574,127 and 6,162,877. Compared to many existing associative thickeners (see US Patent No. 5,574,127), these polymers were useful as rheology modifiers for highly filled aqueous systems at very high  
10       pHs to provide the desired properties. However, like many high molecular weight associative thickeners, these polymers exhibit high viscosity at high solids solutions in water. Consequently, their use in many commercial applications is restricted.

15           Therefore, to widen the utility of these associative thickeners, it is desirable to develop means to lower their high solids solution viscosity. The present invention is directed to address this issue.

#### **SUMMARY OF THE INVENTION**

20           The present invention is directed to a composition comprising a dry blend of a) a hydrophobically modified polyacetal-polyether (HM-PAPE) or comb HM-PAPE and b) a viscosity suppressing agent selected from cyclodextrins and derivatives thereof. Optionally, this dry blend can be heated to fuse the materials together to form a solid mass.

25           This invention also relates to a method for improving the pumpability and pourability of aqueous solutions of HM-PAPE or comb HM-PAPE comprising admixing a cyclodextrin with the HM-PAPE or comb HM-PAPE to form a complex of the cyclodextrin and HM-PAPE or comb HM-PAPE where the  
30       viscosity of the HM-PAPE or comb HM-PAPE is suppressed and adding the complexed admixture to an aqueous system containing a water-insoluble polymer wherein the cyclodextrin is decomplexed and the HM-PAPE or comb HM-PAPE becomes an effective thickener.

## DETAILED DESCRIPTION OF THE INVENTION

It has been surprisingly found that blends of HM-PAPE and cyclodextrin can make a high solids, low viscosity blend that when added to an aqueous medium can form pumpable and pourable slurries or solutions at low water concentrations all the way up to substantially clear homogeneous solutions at medium to high water concentrations.

The polymers of this invention are substantially completely soluble in water at ambient temperatures and have been found to efficiently thicken various water-based systems including latex paints. They also provide an improved combination of paint properties (stability, flow and leveling, film build, spatter resistance, and sag resistance). These polymers are associative thickeners that have a backbone of poly(acetal- or ketal-polyether) with ends that are capped with hydrophobic groups independently selected from the group of alkyl, aryl, arylalkyl, cycloaliphatic, perfluoroalkyl, carbosilyl, polycyclyl, and complex dendritic groups. The hydrophobe content of the polymers of this invention has a lower limit of 8 carbons, preferably 10 carbons, and more preferably 12 carbons. The upper limit of the hydrophobe content is generally 40 carbons, preferably 28 carbons, and more preferably 18 carbons. These polymers are called hydrophobically modified polyacetal-polyether (HM-PAPE) and are marketed by Hercules Incorporated, Wilmington, Delaware, under the trademark Aquaflow.

According to the present invention, the HM-PAPEs are prepared by copolymerizing an alpha, omega-diol, -dithiol, or -diamino polyether or a mixture of these reagents with a gem-dihalide compound in the presence of a base to form an alpha, omega-diol, -dithiol, or -diamino poly(acetal- or ketal-polyether) which in turn is reacted with hydrophobic reagents to form the final product.

The hydrophobically modified comb polymers also have poly(acetal- or ketal-polyether) backbone with pendant hydrophobes. These comb polymers are prepared by 1) copolymerizing water-soluble polymers bearing alpha,

omega-active hydrogen, 2) hydrophobic compounds having alpha, omega-active hydrogen atoms or their alkoxylated derivatives, and 3) dihalogeno compounds or their derivatives in the presence of a base for a sufficient time. Additionally, the ends of these polymers are capped with hydrophobes. As in the HM-PAPE, the hydrophobe content of the comb HM-PAPE polymers of this invention has a lower limit of 8 carbons, preferably 10 carbons, and more preferably 12 carbons. The upper limit of the hydrophobe content is generally 40 carbons, preferably 20 carbons, and more preferably 18 carbons

The HM-PAPes and comb HM-PAPes are described in more detail in US Patent Nos. 5,574,127 and 6,162,877, respectively, the disclosure of which is herein incorporated by reference.

Cyclodextrins (CDs) are cyclic oligosaccharides with six to twelve alpha-D-anhydroglucose units connected together by alpha-(1,4) linkages. They are well known in the art and commercially available. The cyclodextrins composed of six, seven and eight anhydroglucose rings are referred to as alpha ( $\alpha$ )-, beta ( $\beta$ )- and gamma ( $\gamma$ )-cyclodextrin respectively. These truncated cone-shaped molecules are characterized by having a hydrophobic cavity and a relatively hydrophilic exterior. One of the unique properties of CDs is their ability to include appropriate hydrophobic compounds in their cavity to form host-guest complexes.

Cyclodextrins are produced from starch of any selected plant variety, such as corn, potato, waxy maize, and the like which may be modified or unmodified starch derived from cereal or tuber origin and the amylose or amylopectin fractions thereof. The selected starch in the form of an aqueous slurry, at concentrations up to about 35% by weight solids, is usually liquefied, by gelatinization or treatment with a liquefying enzyme such as bacterial alpha-amylase enzyme, and then subjected to treatment with a glycosyltransferase to form the cyclodextrins. The amount of individual alpha-, beta-, and gamma-cyclodextrin formed will vary depending on the selected starch, selected glycosyltransferase and processing conditions. Precipitation and separation of

the individual cyclodextrins are described in the literature using solvent systems, inclusion compounds such as trichloroethylene and non-solvent systems using selected ion exchange resins. Each of the cyclodextrins as well as mixtures thereof is commercially available. Beta-cyclodextrin is by far the most widely  
5 used form and is known for use in the production of pharmaceuticals and foods.

The property of cyclodextrin molecules that makes them useful for the present invention is that the molecule has an apolar, hydrophobic cavity which can contain hydrophobic molecules called guest molecules (or the hydrophobic  
10 portions of amphiphilic molecules) of appropriate sizes to fit inside the cavity and thus form inclusion complexes. One would therefore be led to believe that polar solvents would not have a sufficient affinity for the cavity and would not displace the more hydrophobic guests. In the search for a compatible, nondestructive, liquid or meltable carrier for the cyclodextrin complexes it has been found that  
15 most polar solvents, e.g., the hydroxy and polyhydroxy solvents, e.g., low molecular weight alcohol, ethylene glycol, 1,2-propanediol, glycerol and molten sorbitol, at least partially decompose the inclusion complexes and release some of the guest molecules. Surprisingly, it is now found that some liquid or meltable solids, as described hereinafter, can be used to make pumpable, fluid slurries of  
20 cyclodextrin complexes at typical process temperatures, e.g., at about 100-120°C or lower, without decomposing the cyclodextrin complexes.

Because of this property of the cyclodextrin to form complexes with hydrophobic species, hydrophobic moieties of associative thickeners can bind  
25 (get capped) with CDs. The binding of cyclodextrin compounds with the hydrophobic moieties of associative thickeners disrupts the intermolecular hydrophobic associations and causes a suppression of the viscosity of an aqueous solution containing the associative thickener. The cyclodextrin compounds can then be readily dissociated or decomplexed from the associative  
30 thickener by the addition of another material which has a greater affinity for the cyclodextrin or by dilution with water.

The beta-cyclodextrin and its ethoxylated and propoxylated derivatives are useful in latex paint formulation for achieving a variety of effects, such as for example: to permit the preparation and supply of a low viscosity, high solids solution of the thickener without the use of viscosity suppressing solvent;  
5 improving the ease of incorporating hydrophobically modified associative thickeners, having marginal solubility in water, into aqueous systems; to reduce the viscosity drop of associative thickeners containing formulations upon the addition of colorants or surfactants to the formulation; to improve the efficiency of the associative thickener itself, thus reducing the thickeners required to reach a  
10 given paint viscosity; to reduce foaming in a paint, with or without an associative thickener, which is especially desirable when the paint is to be applied by a roller; and to reduce the color development problems caused by surfactants in some formulations.

15 Materials that have an affinity for the cyclodextrin and that cause the decomplexing or desorbing of the cyclodextrin from the HM-PAPE in the aqueous water-insoluble polymer system are surfactants (i.e., nonionic, cationic, and anionic). These surfactants are readily available in latex formulations. Other solvents that have an affinity for cyclodextrin are hydroxyl-containing  
20 materials such as alcohols. Ethanol is a good example of such an alcohol.

According to the present invention, normally the lower limit of the solids content of the HM-PAPE and/or the comb HM-PAPE in the composition is 3 % by weight of the composition, preferably 7 %, and more preferably 10 %. The  
25 upper limit of the polymer solid content is 35 % by weight, preferably 25 % by weight, and more preferably 20 % by weight. Generally, the cyclodextrin content lower limit is 0.2 % by weight based on the total weight of the composition, preferably 0.5 % by weight, and more preferably 0.7 % by weight. The upper limit of the cyclodextrin is generally 7.0 % by weight, preferably 3.0 %, by weight,  
30 and more preferably 1.5 % by weight.

According to the present invention, in aqueous solutions containing low concentrations of HM-PAPE solids, for example on the order of about 3% by



weight, it was found that the unmodified cyclodextrins, including beta-cyclodextrin, are effective viscosity suppressing additives, while in aqueous solutions containing high concentrations of HM-PAPE solids, for example on the order of greater than about 10% by weight, it was found that the modified  
5 cyclodextrins, having increased water solubility on the order of about 50 grams per 100 grams water, are preferred.

In accordance with this invention, the amount of the cyclodextrin species needed to form a target solution depends on the type of HM-PAPE, its  
10 concentration in solution and the type of cyclodextrin used to suppress the solution viscosity. Cyclodextrin or cyclodextrin derivatives having water-solubility greater than 0.1% can be used to practice the present invention. Examples of water-soluble cyclodextrin derivatives include methylated, hydroxyethylated, hydroxypropylated, carboxymethylated, and diaminoethylated cyclodextrins. The  
15 cyclodextrin derivatives can be nonionic, cationic and anionic. Other hydrophilic cyclic molecules, such as calixarenes, having hydrophobic cavity and ability to complex with the hydrophobes of associative thickeners can also be used.

In accordance with this invention, the HM-PAPE and comb HM-PAPE  
20 compositions can be used in film forming coating compositions such as latex paints, the pigment volume concentration (PVC) of the latex paint can have a lower limit of 15, preferably 24, and more preferably 35 %. The upper limit of the PVC is normally 85, preferably 65 %. According to the jargon of the paint industry, when the latex paint is a high gloss paint, the PVC is from about 15 %  
25 to about 30%; when the paint is a semi-gloss paint, the PVC is from about 20 to about 35 %; and when it is a flat paint, the PVC is from about 40 to about 80 %. Also, for latex paints the ICI viscosity should be above about 1.5 Pa.s at 25°C, for good performance.

30 The basic latex paint contains besides the latex, pigments, fillers, surfactants, cosolvents, and thickeners. Other additives that can be included in paint formulations, for example, are biocides, dispersants, coalescing agents, preservatives, defoamers, and wet-edge agents.

## EXAMPLES

The viscosity of all the solutions in the following Examples was measured using a digital Brookfield viscometer (Model LVDV-1+) at 25°C at 30 rpm unless  
5 mentioned otherwise. All percentages and parts are by weight unless otherwise mentioned.

### EXAMPLE 1

#### 10 Preparation of a solid blend of HM-PAPE and methylated $\beta$ -cyclodextrin

This Example shows how by intimately blending methylated  $\beta$ -cyclodextrin with a HM-PAPE, the solution viscosity of the latter can be lowered.

Aquaflow<sup>TM</sup> NLS-200 HM-PAPE solid (1000 g) (available from Hercules  
15 Incorporated, Wilmington, Delaware) and methylated beta-cyclodextrin (50 g) (available from Cerestar USA, Inc., Hammond, Indiana) were added to a ribbon blender and the resulting mixture heated under a nitrogen atmosphere at 110°C for 1 hour with constant agitation. After that the molten mass was discharged and cooled to room temperature, a homogeneous solid was obtained. There  
20 was no change in the molecular composition (molecular weight and hydrophobe content) of the HM-PAPE after it was heated with methylated beta-cyclodextrin.

The HM-PAPE/ methylated beta-cyclodextrin blend was ground to fine particles and its solubility behavior was tested. It dissolved rapidly in water  
25 without lumping or foaming to form a smooth solution. The 15% solids solution Brookfield viscosity of the blend was 668 cps. By contrast, in the absence of methylated beta-cyclodextrin, the HM-PAPE lumped, took a longer time to dissolve and caused foaming. The lower solution viscosity of the blend relative to that of the pure HM-PAPE (15% solution Brookfield viscosity >20,000 cps)  
30 clearly showed that by adding methylated beta-cyclodextrin, the viscosity of the HM-PAPE could be drastically lowered.

### Example 2

This Example demonstrates the efficacy of hydroxypropylated beta-cyclodextrin to lower the viscosity of Aquaflow NHS-300 HM-PAPE.

Aquaflow NHS-300 HM-PAPE solid (available from Hercules Incorporated, Wilmington, Delaware) (20 g) was dissolved in water (80 g) and the solution pH adjusted to 7.5. To this solution various amounts of hydroxypropylated beta-cyclodextrin (HP- $\beta$ -CD) (available from Cerestar USA, Inc., Hammond, Indiana) were added. The results are shown in Table 1, below.

**TABLE 1**

<b>Amount of HP-<math>\beta</math>-CD added (gram)</b>	<b>Solution BF viscosity @ 26°C (cps)</b>
0.5	5950
0.6	2780
1.0	1580
1.5	940
2.0	560
2.75	360

As can be seen from data in the table, the solution viscosity of Aquaflow (R) NHS-300 HM-PAPE steadily decreased as the amount of HP- $\beta$ -CD was increased.

### **Example 3**

This Example shows the efficacy of beta-cyclodextrin to lower the viscosity of high solids solution of Aquaflow <sup>(TM)</sup> NHS-300 HM-PAPE.

Aquaflow <sup>(TM)</sup> NHS-300 HM-PAPE solid (20 g) was dissolved in water (80 g) and the solution pH was adjusted to 7.5. To this solution various amounts of beta-cyclodextrin ( $\beta$ -CD) (available from Cerestar USA, Inc., Hammond, Indiana) were added. The results are shown in Table 2, below.

TABLE 2

Amount of $\beta$ -CD added (gram)	Solution BF viscosity (cps)
0	5950
0.50	2508
1.0	1268
1.5	775
2.0	533
3.0	242
4.0	200

As can be seen from data in the above Table 2, the solution viscosity of Aquaflow(TM) NHS-300 HM-PAPE steadily decreased as the amount of  $\beta$ -CD was increased.

#### Example 4

This Example shows the efficacy of methylated beta-cyclodextrin to lower the viscosity of high solids (20%) solution of Aquaflow(TM) NHS-300 HM-PAPE.

Aquaflow (TM) NHS-300 HM-PAPE solid (20 g) was dissolved in water (80 g) and the solution pH adjusted to 7.5. To this solution various amounts of methylated beta-cyclodextrin (Me- $\beta$ -CD) were added. The results are shown in Table 3, below.

TABLE 3

Amount of Me- $\beta$ -CD added (gram)	Solution BF viscosity (cps)
0	5950
0.50	1956
1.0	952
1.5	485
2.0	308

As can be seen from data in the above Table 3, the solution viscosity of Aquaflow(TM) NHS-300 HM-PAPE steadily decreased as the amount of Me- $\beta$ -CD was increased.

### Example 5

This Example shows the efficacy of methylated beta-cyclodextrin to lower the viscosity of high solids (25%) solution of Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE.

5 Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE solid (25.3g; "as is") was dissolved in water (75 g). To this solution various amounts of methylated beta-cyclodextrin (Me- $\beta$ -CD) was added. The results are shown in Table 4, below.

**TABLE 4**

<b>Amount of Me-<math>\beta</math>-CD added (gram)</b>	<b>Solution BF viscosity @ 28°C (cps)</b>
0	14220
1.0	1970
1.5	1288
2.0	920
2.5	645

10

As can be seen from data in Table 4, the 25% solids solution viscosity of Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE steadily decreased as the amount of Me- $\beta$ -CD was increased.

15

### Example 6

This Example shows the efficacy of methylated beta-cyclodextrin to lower the viscosity of high solids solution of an Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE.

20 Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE solid (available from Hercules Incorporated, Wilmington, Delaware) (17.5 g; "as is") was dissolved in water (83 g). To this solution various amounts of methylated beta-cyclodextrin (Me- $\beta$ -CD) were added. The results are shown in Table 5, below.

TABLE 5

Amount of Me- $\beta$ -CD added (gram)	Solution BF viscosity @ 28°C (cps)
0	>20,000
0.56	6940
0.79	4500
1.19	2328
1.49	1580
1.84	930

As can be seen from data in Table 5, the solution viscosity of Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE steadily decreased as the amount of Me- $\beta$ -CD was increased.

#### Example 7

This Example shows the efficacy of beta-cyclodextrin to lower the viscosity of high solids solution of an Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE.

Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE solid (17.5 g; "as is") was dissolved in water (83 g). To this solution various amounts of beta-cyclodextrin ( $\beta$ -CD) were added. The results are shown in Table 6, below.

TABLE 6

Amount of $\beta$ -CD added (gram)	Solution BF viscosity @ 35°C (cps)
0	>20,000
0.6	>20,000
1.0	16450
2.02	5300
3.02	1450

As can be seen from data in Table 6, the solution viscosity of Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE steadily decreased as the amount of  $\beta$ -CD was increased.

#### Example 8

This Example shows the efficacy of hydroxypropylated beta-cyclodextrin to lower the viscosity of high solids solution of an Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE.

Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE solid (17.5 g; "as is") was dissolved in water (83 g). To this solution various amounts of hydroxypropylated beta-cyclodextrin (HP- $\beta$ -CD) were added. The results are shown in Table 7, below.

5

**TABLE 7**

Amount of HP- $\beta$ -CD added (gram)	Solution BF viscosity @ 35°C (cps)
0	>20,000
0.56	>20,000
1.0	15,800
1.5	9080
2.0	6080
2.75	3340
3.35	1980

As can be seen from data in Table 7, the solution viscosity of Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE steadily decreased as the amount of HP- $\beta$ -CD was increased.

10

High solids solutions (>15%) of Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE using HP- $\beta$ -CD were also made and evaluated in the Rhoplex AC-417M all-acrylic semi-gloss paint. It was found that the basic rheological properties of Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE delivered in conjunction with HP- $\beta$ -CD were equivalent to those for the same Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE delivered using 4:1 water/butyl carbitol mixture.

15

### Example 9

This Example shows the efficacy of methylated beta-cyclodextrin to lower the viscosity of high solids (17%) solution of an Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE.

20

Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE solid (17.5 g; "as is") was dissolved in water (83 g). To this solution various amounts of methylated beta-cyclodextrin (Me- $\beta$ -CD) were added. The results are shown in Table 8, below.

25

TABLE 8

Amount of Me- $\beta$ -CD added (gram)	Solution BF viscosity @ 28°C (cps)
0	>20,000
0.56	6940
0.79	4500
1.19	2328
1.49	1580
1.84	930

As can be seen from data in Table 8, the solution viscosity of Aquaflow<sup>(TM)</sup>  
 5 NLS-200 HM-PAPE steadily decreased as the amount of Me- $\beta$ -CD was  
 increased.

### Example 10

This Example shows the efficacy of hydroxypropylated beta-cyclodextrin  
 10 to lower the viscosity of high solids (17%) solution of an Aquaflow<sup>(TM)</sup> NLS-200  
 HM-PAPE.

Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE solid (17.5 g; "as is") was dissolved in  
 water (83 g). To this solution various amounts of hydroxypropylated beta-  
 15 cyclodextrin (HP- $\beta$ -CD) were added. The results are shown in Table 9, below.

TABLE 9

Amount of HP- $\beta$ -CD added (gram)	Solution BF viscosity @ 35°C (cps)
0	>20,000
0.56	>20,000
1.0	15,800
1.5	9080
2.0	6080
2.75	3340
3.35	1980

As can be seen from data in Table 9, the solution viscosity of Aquaflow<sup>(TM)</sup>  
 20 NLS-200 HM-PAPE steadily decreased as the amount of HP- $\beta$ -CD was  
 increased.



### Example 11

This Example shows the efficacy of methylated beta-cyclodextrin to lower the viscosity of high solids solution of an Aquaflow<sup>(TM)</sup> NLS-210 HM-PAPE.

Aquaflow<sup>(TM)</sup> NLS-210 HM-PAPE solid (available from Hercules Incorporated, Wilmington, Delaware) (17.4 g; "as is") was dissolved in water (83 g). To this solution various amounts of methylated beta-cyclodextrin (Me- $\beta$ -CD) were added. The results are shown in Table 10, below.

TABLE 10

Amount of Me- $\beta$ -CD added (gram)	Solution BF viscosity @ 26°C (cps)
0	>20,000
0.8	5940
1.3	3440
1.7	2200
2.1	1392
2.5	796

As can be seen from data in Table 10 above, the solution viscosity of Aquaflow<sup>(TM)</sup> NLS-210 HM-PAPE steadily decreased as the amount of Me- $\beta$ -CD was increased.

### Example 12

This Example shows the efficacy of hydroxypropylated beta-cyclodextrin to lower the viscosity of high solids solution of an Aquaflow<sup>(TM)</sup> NLS-210 HM-PAPE.

Aquaflow<sup>(TM)</sup> NLS-210 HM-PAPE solid (17.4 g; "as is") was dissolved in water (83 g). To this solution various amounts of hydroxypropylated beta-cyclodextrin (HP- $\beta$ -CD) were added. The results are shown in Table 11, below.

TABLE 11

Amount of HP- $\beta$ -CD added (gram)	Solution BF viscosity @ 36°C (cps)
0	>20,000
2.0	>15,000
3.0	8400
4.0	5700
2.0	6080
5.0	2680
6.0	1210

As can be seen from data in Table 11 above, the solution viscosity of Aquaflow<sup>TM</sup> NLS-210 HM-PAPE steadily decreased as the amount of HP- $\beta$ -CD was increased.

### Example 13

This Example shows the efficacy of various  $\beta$ -cyclodextrins to lower the viscosity of hydrophobically modified comb polyacetal-polyethers.

10

The hydrophobically modified comb polymer used in these experiments was made as described below.

To an Abbe ribbon blender were added polyethylene glycol (MW~ 8000) (PEG-8000) (1000 g), 1-hexadecylamine (8 g), and sodium hydroxide (34 g). After sealing the reactor, the mixture was heated at 80°C for one hour. Then dibromomethane (20.4 g) was added to the PEG-8000/1-hexadecylamine/NaOH mixture and the resulting reaction mixture heated at 80°C for four hours to form the resulting comb copolymer. To this comb polymer at 80°C was added 1-bromohexadecane (70 g) and the resulting reaction mixture heated at 120°C for two hours. Following this, the reactor was opened and the molten reaction mixture was poured into a plastic tray. After cooling to room temperature, the reaction mixture solidified. The weight average molecular of the copolymer was 58,300 with a polydispersity index of 1.96. The 2% aqueous solution Brookfield viscosity of the copolymer was 520 cps.

25

To an aqueous solution (100g) (polymer content ~ 9.8 %) of this copolymer, various amounts of  $\beta$ -cyclodextrin, hydroxypropylated  $\beta$ -cyclodextrin

and methylated  $\beta$ -cyclodextrin were added and the mixture was mixed till the added cyclodextrin dissolved. The viscosities in the presence of various types and amounts of  $\beta$ -cyclodextrins are shown in Table 12, below.

TABLE 12

Amount of cyclodextrin (CD) added (g)	Brookfield viscosity in the presence of $\beta$ -CD <sup>a</sup> (cps)	Brookfield viscosity in the presence of HP- $\beta$ -CD <sup>b</sup> (cps)	Brookfield viscosity in the presence of Me- $\beta$ -CD <sup>c</sup> (cps)
0	>20,000	>20,000	>20,000
0.5	2168	4880	665
1.0	321	1172	115
1.5	66	270	62

<sup>a</sup>  $\beta$ -CD =  $\beta$ -Cyclodextrin;

<sup>b</sup> HP- $\beta$ -CD = Hydroxypropylated  $\beta$ -cyclodextrin;

<sup>c</sup> Me- $\beta$ -CD = Methylated  $\beta$ -cyclodextrin

As can be seen from Table 12 above, the hydrophobically modified comb polymer underwent significant viscosity loss in the presence of various  $\beta$ -cyclodextrins.

#### Example 14

The hydrophobically modified comb polymer used in these experiments was made by copolymerizing polyethylene glycol (MW~ 8000) (1000 g), RHODAMEEN T-50 (available from Rhodia, Inc., New Jersey) (44.5 g), dibromomethane (17.1 g) in the presence of sodium hydroxide (35 g) and then reacting the resulting comb copolymer with 1-bromohexadecane (90 g) according to the reaction conditions described in Example 13, above. The weight average molecular of the comb copolymer was 38,100 with a polydispersity index of 1.83. The 2% aqueous solution Brookfield viscosity of the copolymer was 665 cps.

To an aqueous solution (100g) (polymer content ~ 9.7 %) of this copolymer, various amounts of  $\beta$ -cyclodextrin and hydroxypropylated  $\beta$ -cyclodextrin were added and the mixture was mixed till the added cyclodextrin

dissolved. The viscosities in the presence of various amounts of  $\beta$ -cyclodextrin and hydroxypropylated  $\beta$ -cyclodextrin are shown below.

**TABLE 13**

Amount of cyclodextrin (CD) added (g)	Brookfield viscosity in the presence of $\beta$ -CD (cps)	Brookfield viscosity in the presence of HP- $\beta$ -CD (cps)
0	>20,000	>20,000
0.5	19886	15860
1.0	4400	980
2.0	215	980
3.0	68	150

As can be seen from Table 13 above, the aqueous solution of the hydrophobically modified comb polymer underwent significant viscosity loss as increasing amount of  $\beta$ -cyclodextrin and hydroxypropylated  $\beta$ -cyclodextrin was added.

**Example 15**

The hydrophobically modified comb polymer used in these experiments was made using the following reagents:

- a) PEG-8000 – 1000 g,
- b) RHODAMEEN T-50 – 44.5 g, (available from Rhodia, Inc., New Jersey)
- c) Sodium hydroxide – 35 g,
- d) Dibromomethane – 19 g, and
- e) 1-Bromohexadecane – 100 g.

The reaction conditions were the same as those described in Example 13 above.

To an aqueous solution (100g) (polymer content ~ 9.6 %) of this copolymer, various amounts of  $\beta$ -cyclodextrin and hydroxypropylated  $\beta$ -cyclodextrin were added and the mixture was mixed till the added cyclodextrin dissolved. The viscosities in the presence of various amounts of  $\beta$ -cyclodextrin and hydroxypropylated  $\beta$ -cyclodextrin are shown in Table 14, below.

**TABLE 14**

Amount of cyclodextrin (CD) added (g)	Brookfield viscosity in the presence of $\beta$ -CD (cps)	Brookfield viscosity in the presence of HP- $\beta$ -CD (cps)
0	>20,000	>20,000
0.5	1884	3500
1.0	408	822
2.0	250	328

As can be seen from Table 14 above, the aqueous solution of the hydrophobically modified comb polymer underwent significant viscosity loss as increasing amount of  $\beta$ -cyclodextrin and hydroxypropylated  $\beta$ -cyclodextrin was added.

**Example 16**

This Example demonstrates the efficacy of  $\alpha$ -cyclodextrin ( $\alpha$ -CD) to lower the viscosity of Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE.

Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE solid (available from Hercules Incorporated, Wilmington, Delaware) (20 g) was dissolved in water (80 g). To this solution were added various amounts of  $\alpha$ -CD (available from Cerestar USA, Inc., Hammond, Indiana). The results are shown in Table 15, below.

**TABLE 15**

Amount of $\alpha$ -CD added (gram)	Solution BF viscosity @ 26°C (cps)
0.30	3340
0.60	2072
0.90	1264

As can be seen from data in Table 15 above, the solution viscosity of Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE steadily decreased as the amount of  $\alpha$ -CD was increased.

**Example 17**

This Example demonstrates the efficacy of  $\gamma$ -cyclodextrin ( $\gamma$ -CD) to lower the viscosity of Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE.

Aquaflow<sup>TM</sup> NLS-200 HM-PAPE solid (available from Hercules Incorporated, Wilmington, Delaware) (10 g) was dissolved in water (90 g). To this solution were added various amounts of  $\gamma$ -CD (available from Cerestar USA, Inc., Hammond, Indiana). The results are shown in Table 16, below.

5

TABLE 16

Amount of $\gamma$ -CD added (grams)	Solution BF viscosity (cps)
0	>20,000
0.30	>20,000
0.60	17,480
0.90	12,300
1.20	9,340
1.50	7,200
1.80	4,580

As can be seen from data in Table 16 above, the solution viscosity of Aquaflow<sup>TM</sup> NLS-200 HM-PAPE steadily decreased as the amount of  $\gamma$ -CD was increased.

10

#### Paint properties of cyclodextrin-containing HM-PAPEs

The appropriate cyclodextrin-containing HM-PAPE solution was incorporated into a flat, eggshell and high gloss paint formula to achieve an initial Stormer viscosity of 90-95 Kreh Units. The ingredients used in these formulas are described below. The significance and scale of various paint properties are as follows:

15

- a) Stormer viscosity (initial and after overnight storage) (I/O) is measured by a Stormer viscometer at 200 sec<sup>-1</sup> shear rate and expressed in Kreh Units (KUs).
- b) ICI viscosity is measured by an ICI plate and cone viscometer at 12,000 sec<sup>-1</sup> and expressed in poise.
- c) Thickening efficiency (TE) is measured as dry weight % thickener in the paint to achieve the initial Stormer viscosity.
- d) Leveling by Leneta method (measured on a scale 0-10; 0 = worst; and 10 = best).

20

25

- e) Sag resistance by Leneta method, mid range bar, wet film thickness (WFT) (in mils) above which sag occurs.
- f) Spatter resistance by roll-out over a black panel (compared on scale of 0-10; 0 = worst and 10 = best).
- g) 60° Gloss is specular gloss viewed at 60°.

**EXAMPLE 18**  
**UCAR® 367 vinyl-acrylic latex based interior flat paint formula**

A high solids solution was made by dissolving 18.3 g ("as is") of Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE solid in a solution of hydroxypropylated  $\beta$ -cyclodextrin (5 g) in water (83 g). The resulting polymer solution was evaluated in a UCAR® 367 vinyl-acrylic latex based interior flat paint formula described in US patent No. 5,879,440. The paint properties of this thickener solution against a control Aquaflow<sup>(TM)</sup> NLS-200 HM-PAPE solution (25 g of the polymer dissolved in 1:4 (w/w) mixture of butyl carbitol and 75 g of water) are compared below in Table 17.

**TABLE 17**

Thickener	TE (wt%)	KU (I/O)	ICI Viscosity (poise)	Leveling	Sag resistance	Spatter
Aquaflow(TM) NLS-200 (control)	0.50	94/109	2.3	9	6	9
Cyclodextrin-containing Aquaflow(TM) NLS-200	0.50 <sup>a</sup>	93/110	2.4	9	6	9

<sup>a</sup> TE based on the pure HM-PAPE

As can be seen from above results in Table 17, the performances of the HM-PAPE were not adversely affected in the presence of hydroxypropylated  $\beta$ -cyclodextrin.

**EXAMPLE 19**  
**UCAR® 379/UCAR 625 Vinyl-acrylic/acrylic eggshell paint formula**

The above thickener solutions were also evaluated in UCAR 367/UCAR 625 (vinyl-acrylic/acrylic) eggshell paint formula. The details of the UCAR 367/625 eggshell paint formula are given in TABLE 18 below.

**TABLE 18****Base Paint (pigment grind)**

Ingredient	Grams/1000 grams	Manufacturer
Water	113.6	
Nuosept-95 Preservative	2.35	Hüls America, New Jersey
Tamol 731 (Dispersant)	9.4	Rohm & Haas Company, Pennsylvania
Triton N-57 surfactant (Dispersant)	2.4	The Dow Chemical Company, Michigan
2-Amino-2-methyl-1-propanol (AMP-95)	1.0	The Dow Chemical Company, Michigan
Propylene glycol	52.8	The Dow Chemical Company, Michigan
Colloid-643 Antifoam	1.9	Rhodia, Inc., New Jersey
Water, Discretionary (as needed for effective dispersion)		
Ti-Pure ® R-900 titanium dioxide	229.3	E. I. DuPont de Nemours & Co., Delaware
Optiwhite pigment	102	Burgess Pigment co., Georgia
Burgess No. 98 pigment	25.5	Burgess Pigment co., Georgia

Disperse to Hegman 4 to 5 and letdown at slower speed.

5

**Letdown**

Ingredient	Amount (grams)	Manufacturer
UCAR® Filmer IBT	12	The Dow Chemical Company, Midland, Michigan
UCAR® 379 Vinyl-acrylic latex	319.5	The Dow Chemical Company, Midland, Michigan
UCAR® 625 Acrylic latex	113.2	The Dow Chemical Company, Midland, Michigan
Butyl Carbitol ® coalescent	12	The Dow Chemical Company, Midland, Michigan
Colloid-643 Antifoam	2.9	Rhodia, Inc., New Jersey

The above base paint (230 g) was mixed with an appropriate amount (15 g) of water/thickener solution to adjust the Stormer viscosity of the paint to 97±2 KU. The paint properties of the thickeners are given in Table 20, below.

10

**TABLE 20**

Thickener	TE (wt%)	KU (I/O)	ICI Viscosity (poise)	Leveling	Sag resistance	Spatter
Aquaflow(TM) NLS-200 (control)	0.53	97/113	3.2	9	12	9
Cyclodextrin-containing Aquaflow(TM) NLS-200	0.54 <sup>a</sup>	94/109	3.1	9	10	9

<sup>a</sup> TE based on the pure HM-PAPE



As can be seen from above results in Table 20, the performances of the HM-PAPE were not adversely affected in the presence of hydroxypropylated  $\beta$ -cyclodextrin.

5

**EXAMPLE 20****Rhoplex HG-74P styrene-acrylic high gloss paint formula**

A high solids solution was made by dissolving 20.3 g ("as is") of Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE solid in solutions of various types of  $\beta$ -cyclodextrins (1.0-1.5 g) in water (80 g). The resulting polymer solutions were evaluated in the above Rhoplex HG-74P styrene-acrylic latex based high gloss paint formula. The paint properties of these cyclodextrin-containing thickener solutions were compared against those of a control Aquaflow<sup>(TM)</sup> NHS-300 HM-PAPE solution (20.3 g of the polymer dissolved in 80 g of water).

15

The details of the Rhoplex HG-74P styrene-acrylic high gloss paint formula are given in TABLE 21 below.

**TABLE 21**

Ingredients	Pounds	Gallons	Manufacturer
Water	40.00	4.80	
Propylene Glycol	45.00	5.19	The Dow Chemical Co., Midland, Michigan
Butyl Carbitol	32.00	4.00	The Dow Chemical Co., Midland, Michigan
Proxel GXL	2.00	0.24	The Dow Chemical Co., Midland, Michigan
Rhodamine 111M	12.00	1.30	Rhodia, Inc., New Jersey
Triton CF-10	2.00	0.22	The Dow Chemical Co., Midland, Michigan
Colloid 640	2.00	0.26	Rhodia, Inc., New Jersey
2-Amino-2-methyl-1-propanol (AMP-95)	1.00	0.13	The Dow Chemical Co., Midland, Michigan
Strodex PK-90	1.00	0.11	Dexter, Illinois
Tronox CR-828	225.00	6.60	Kerr-McGee, Oklahoma City, Oklahoma

Grind to Hegman >8 and letdown at slower speed to the mixture of ingredients shown below.

Letdown	Rhoplex HG-74P Styrene-acrylic latex	620.00	69.66	Rohm & Haas Company, Philadelphia, Pennsylvania
	Colloid 640	2.00	0.26	Rhodia, Inc., New Jersey
	Post addition premix	60.00	7.20	
	<b>Total</b>	<b>1044.00</b>	<b>100.0</b>	

**Formula Constants**

Pigment volume concentration, %	19.94
Nonvolatile volume, %	33.1
Nonvolatile weight, %	46.5
Coalescent on latex, %	12.3
Dispersant on pigment, %	1.3

The above base paint (246 pounds) set forth in Table 21 was thickened with thickener/water mixture (15 pounds) to achieve an initial Stormer viscosity of 95±5 KU. The paint properties of the cyclodextrin-free (control sample) and cyclodextrin-containing Aquaflow<sup>(TM)</sup> NHS-300 solutions are shown in Table 22, below.

TABLE 22

Thickener	Cyclodextrin type /amount (g)	TE <sup>a</sup> (wt%)	KU (I/O)	ICI Viscosity (poise)	Leveling	Sag resistance	Spatter	60° Gloss
Aquaflow <sup>(TM)</sup> NHS-300 (control)	—	0.30	98/98	3.2	10	6	9	75
Cyclodextrin-containing Aquaflow <sup>(TM)</sup> NHS-300	@-CD/1.0	0.30	97/98	3.2	10	8	9	74
"	HP-@-CD/1.5	0.30	97/97	3.1	10	6	9	76
"	Me-@-CD/1.0	0.30	96/97	3.1	10	6	9	73

<sup>a</sup> TE based on solids content of the thickener solution.

As can be seen from above results in Table 22, the performances of the cyclodextrin-containing Aquaflow<sup>(TM)</sup> NHS-300 were not adversely affected in the presence of various types of cyclodextrins.

Although this invention has been described with respect to specific embodiments, it should be understood that these embodiments are not intended to be limiting and that many variations and modifications are possible without departing from the spirit and scope of this invention.

## WHAT IS CLAIMED IS:

1. A composition comprising
  - a) a hydrophobically modified polyacetal-polyether or comb
  - 5 hydrophobically modified polyacetal-polyether and
  - b) a viscosity suppressing agent selected from the group consisting of cyclodextrins and derivatives thereof.
2. The composition of claim 1, wherein the cyclodextrins are selected  
10 from the group consisting of alpha ( $\alpha$ ), beta ( $\beta$ ), and gamma ( $\gamma$ ) cyclodextrins.
3. The composition of claim 1, wherein the cyclodextrin derivatives are selected from the group consisting of methylated, hydroxyethylated, hydroxypropylated, carboxymethylated, and diaminoethylated cyclodextrins  
15
4. The composition of claim 1, wherein the lower limit of the hydrophobe types has 8 carbons.
5. The composition of claim 1, wherein the lower limit of the  
20 hydrophobe types has 10 carbons.
6. The composition of claim 1, wherein the lower limit of the hydrophobe types has 12 carbons.
- 25 7. The composition of claim 1, wherein the upper limit of the hydrophobe types has 40 carbons.
8. The composition of claim 1, wherein the upper limit of the hydrophobe types has 28 carbons.  
30
9. The composition of claim 1, wherein the upper limit of the hydrophobe types has 18 carbons.

10. The composition of claim 1, wherein the lower limit of the solids content of the polymer is 3 wt. %.

5 11. The composition of claim 1, wherein the lower limit of the solids content of the polymer is 7 wt %.

12. The composition of claim 1, wherein the lower limit of the solids content of the polymer is 10 wt %.

10 13. The composition of claim 1, wherein the upper limit of the solids content of the polymer is 35 wt %.

14. The composition of claim 1, wherein the upper limit of the solids content of the polymer is 25 wt %.

15 15. The composition of claim 1, wherein the upper limit of the solids content of the polymer is 20 wt %.

20 16. The composition of claim 1, wherein the lower limit of the cyclodextrin content is 0.2 wt %.

17. The composition of claim 1, wherein the lower limit of the cyclodextrin content is 0.5 wt %.

25 18. The composition of claim 1, wherein the lower limit of the cyclodextrin content is 0.7 wt %.

19. The composition of claim 1, wherein the upper limit of the cyclodextrin content is 7.0 wt %.

30 20. The composition of claim 1, wherein the upper limit of the cyclodextrin content is 3.0 wt %.

21. The composition of claim 1, wherein the upper limit of the cyclodextrin content is 1.5 wt %.

22. The composition of claim 1, wherein the solids content of the polymer is 20 wt % and the cyclodextrin content is 1.0 wt %.

23. The composition of claim 1, wherein the solids content of the polymer is 17 wt % and the cyclodextrin content is 3.0 wt %.

24. A process for preparing the composition of claim 1 comprising dry blending a hydrophobically modified polyacetal-polyether (HM-PAPE) or comb hydrophobically modified polyacetal-polyether (comb HM-PAPE) with a cyclodextrin.

25. The process of claim 24, wherein the blend of dry HM-PAPE or comb HM-PAPE and the cyclodextrin is heated to fuse the materials together to form a solid mass.

26. The process of claim 24, wherein the cyclodextrin is selected from the group consisting of alpha ( $\alpha$ ), beta ( $\beta$ ), and gamma ( $\gamma$ ) cyclodextrins and mixtures thereof.

27. The process of claim 26, wherein the viscosity suppressing agent is selected from the group consisting of methylated, hydroxyethylated, hydroxypropylated, carboxymethylated, and diaminoethylated cyclodextrins and mixtures thereof.

28. A method for improving the incorporation of a thickener of a hydrophobically modified polyacetal-polyether (HM-PAPE) or comb hydrophobically modified polyacetal-polyether (comb HM-PAPE) into an aqueous system containing a water-insoluble polymer comprising

a) admixing a cyclodextrin or cyclodextrin derivative with said thickener in a sufficient amount to effectively complex the thickener so as to keep the

viscosity of the admixture in abeyance,

b) adding said complexed admixture to said aqueous system containing said water-insoluble polymer, and

5 c) adding or providing to said aqueous system containing said complexed admixture and said water-insoluble polymer system an effective amount of a compound having an affinity for the cyclodextrin to decomplex the cyclodextrin from the thickener to increase the viscosity of the system.

29. The method of claim 28, wherein the cyclodextrin is selected from  
10 the group consisting of alpha ( $\alpha$ ), beta ( $\beta$ ), and gamma ( $\gamma$ ) cyclodextrins and mixtures thereof.

30. The process of claim 29, wherein the cyclodextrin is selected from the group consisting of methylated, hydroxyethylated, hydroxypropylated,  
15 carboxymethylated, and diaminoethylated cyclodextrins and mixtures thereof.

31. A paint composition comprising a latex and the composition of claim 1.

20 32. The paint composition of claim 31, wherein the pigment volume concentration (PVC) has a lower limit of about 15 %.

33. The paint composition of claim 31, wherein the pigment volume concentration (PVC) has a lower limit of about 24 %.

25 34. The paint composition of claim 31, wherein the pigment volume concentration (PVC) has a lower limit of about 35 %.

30 35. The paint composition of claim 31, wherein the pigment volume concentration (PVC) has an upper limit of about 85 %.

36. The paint composition of claim 31, wherein the pigment volume concentration (PVC) has an upper limit of about 65 %.

A. CLASSIFICATION OF SUBJECT MATTER  
IPC 7 C08L101/00 C08L71/00 C09D7/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 C08L C09D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 5 574 127 A (SAU ARJUN C) 12 November 1996 (1996-11-12) column 4, line 8-12; claims 1-38 -----	1-36
Y	US 6 162 877 A (SAU ARJUN C) 19 December 2000 (2000-12-19) column 7, line 35-38; claims 1-105 -----	1-36
Y	EP 0 460 896 A (ROHM & HAAS) 11 December 1991 (1991-12-11) claims 1-3 -----	1-36

☐ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

\* Special categories of cited documents :

\*A\* document defining the general state of the art which is not considered to be of particular relevance

\*E\* earlier document but published on or after the international filing date

\*L\* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

\*O\* document referring to an oral disclosure, use, exhibition or other means

\*P\* document published prior to the international filing date but later than the priority date claimed

\*T\* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

\*X\* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

\*Y\* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

\*Z\* document member of the same patent family

Date of the actual completion of the international search

20 January 2003

Date of mailing of the international search report

07/02/2003

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2  
NL - 2280 HV Rijswijk  
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,  
Fax: (+31-70) 340-3016

Authorized officer

Hoffmann, K



Patent document cited in search report		Publication date	Patent family member(s)	Publication date
US 5574127	A	12-11-1996	AU 709801 B2	09-09-1999
			AU 5189996 A	23-10-1996
			CA 2221748 A1	10-10-1996
			CN 1185790 A	24-06-1998
			EP 0820479 A1	28-01-1998
			NZ 304717 A	28-01-1999
			RU 2181365 C2	20-04-2002
			TW 462975 B	11-11-2001
			WO 9631550 A1	10-10-1996
			ZA 9602746 A	07-10-1996
US 6162877	A	19-12-2000	AU 1833500 A	26-06-2000
			BR 9915936 A	21-08-2001
			CN 1329632 T	02-01-2002
			EP 1135428 A1	26-09-2001
			JP 2002531655 T	24-09-2002
			WO 0034361 A1	15-06-2000
EP 0460896	A	11-12-1991	US 5137571 A	11-08-1992
			AT 126817 T	15-09-1995
			AU 652937 B2	15-09-1994
			AU 7812891 A	12-12-1991
			BR 9102314 A	14-01-1992
			CA 2043342 A1	06-12-1991
			CN 1057064 A ,B	18-12-1991
			DE 69112285 D1	28-09-1995
			DE 69112285 T2	21-03-1996
			DK 460896 T3	25-09-1995
			EP 0460896 A2	11-12-1991
			ES 2077801 T3	01-12-1995
			FI 912689 A	06-12-1991
			HK 25896 A	16-02-1996
			IE 911903 A1	18-12-1991
			JP 3055816 B2	26-06-2000
			JP 4227986 A	18-08-1992
			JP 3292299 B2	17-06-2002
			JP 2000178530 A	27-06-2000
			JP 3173603 B2	04-06-2001
			JP 2000178507 A	27-06-2000
			KR 171603 B1	20-03-1999
			NO 912131 A	06-12-1991
			NZ 238387 A	26-10-1993
			PT 97871 A	30-04-1992